# Isotopic Studies of NO<sub>X</sub> Storage and Reduction over Pt/BaO/Al<sub>2</sub>O<sub>3</sub> using Temporal Analysis of Products

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## Introduction

 $NO_X$  Storage and Reduction (NSR) is an emerging technology for  $NO_X$  emission abatement in lean burn gasoline and diesel engines. The  $NO_X$  removal process involves storage of  $NO_X$  on an alkali earth component (Ba, Ca) mediated by precious metals (Pt, Rh) followed by injection of a rich pulse for a shorter duration to reduce the stored  $NO_X$ . In this study, we employ Temporal Analysis of Products (TAP) experiments with isotopic labeling to elucidate the regeneration chemistry. TAP experiments are carried out isothermally in the Knudsen transport regime, thereby avoiding thermal and mass transport complications typical of atmospheric pressure reactors. TAP experiments are carried out utilizing isotopic species on  $Pt/BaO/Al_2O_3$  catalysts with varied Pt loadings and dispersions but an equal number of exposed Pt sites. The use of labeled  $^{18}O_2$  and  $^{15}NO$  provided resolution of reaction pathways such as for  $N_2$  formation during the regeneration step. The experiments help to elucidate the roles of Pt and the coupling between the precious metal and storage phases. .

#### Materials and Methods

Two Pt/BaO/Al<sub>2</sub>O<sub>3</sub> powder catalysts were used having vastly different Pt loading (wt.%) and dispersion, but equal exposed Pt sites (catalysts provided by BASF Inc.; Table 1). While sample D3 was used as provided, sample B2M was a physical mixture of Pt/BaO/Al<sub>2</sub>O<sub>3</sub> and BaO/Al<sub>2</sub>O<sub>3</sub>, the latter of which was added to achieve the requisite BaO sites. The TAP studies involved feeding pulses of the reactant over catalysts over 150°C - 400°C. The feed gas consisted of NO, H<sub>2</sub>, <sup>15</sup>NO (98 atom% <sup>15</sup>N, Cambridge Isotope Laboratories) and <sup>18</sup>O<sub>2</sub> (99 atom% <sup>18</sup>O, Icon Isotopes). The use of labeled <sup>15</sup>NO enabled the probing of pathways to the N-containing products. Effluent species included H<sub>2</sub> (m/e=2), N<sub>2</sub> (m/e=28), <sup>15</sup>NN (m/e=29), <sup>15</sup>N<sub>2</sub> (m/e=30), NO (m/e=30), <sup>15</sup>NO (m/e=31), O<sub>2</sub> (m/e=32), <sup>15</sup>N<sup>18</sup>O (m/e=33), <sup>18</sup>OO (m/e=34), <sup>18</sup>O<sub>2</sub> (m/e=36), and N<sub>2</sub>O (m/e=44) and were monitored with a quadrupole mass spectrometer. Two kinds of experiments are performed: (i) pulse storage experiments, in which NO (or <sup>15</sup>NO) was pulsed with a spacing time of  $\tau_s$ , and (ii) pump-probe NSR experiments in which sequential pulses of NO and H<sub>2</sub> (or <sup>15</sup>NO and H<sub>2</sub>) were pulsed over pre-reduced, pre-oxidized or pre-nitrated catalysts with prescribed delay time ( $\tau_e$ ) and spacing time ( $\tau_e$ ).

Table 1. Physical properties of Pt/BaO/Al<sub>2</sub>O<sub>3</sub> catalyst samples

|                                      | Sample D3            | Sample B2M             |
|--------------------------------------|----------------------|------------------------|
| Pt (wt%)                             | 2.7                  | 0.28                   |
| BaO (wt%)                            | 14.6                 | 16.6                   |
| Pt dispersion (%)                    | 3                    | 33                     |
| Mass of catalyst (mg)                | 110                  | 97                     |
| Estimated number of exposed Pt sites | $2.8 \times 10^{17}$ | 2.8 x 10 <sup>17</sup> |

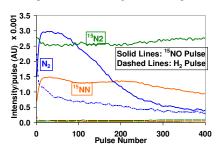
## Results and Discussion

NO pulse storage experiments were carried out at 250 °C on pre-reduced catalyst to compare NO decomposition and storage differences in the two catalysts. The NO storage capacity of the lower dispersion catalyst (D3)) exceeded that of the higher dispersion catalyst (B2M). This suggests that in the physical mixture, the bulk BaO/Al $_2$ O $_3$  does not provide significant NO $_x$  storage. Moreover, catalyst D3 had a higher production of N $_2$  during the initial NO pulses than the higher dispersion catalyst (B2M). This suggests that Pt sites on the larger Pt crystallites are more active for NO decomposition.

Similar experiments with labeled  $^{15}NO$  pulsing on pre-nitrated Pt/BaO/Al $_2O_3$  catalysts (using unlabeled NO) provide evidence for a dynamic equilibrium between the gas and Pt as well as between Pt and BaO. Moreover, the sustained production of  $^{15}N_2$  over hundreds of pulses and a noted absence of  $^{15}NN$  and  $N_2$  products suggest that the  $^{15}N_2$  formation pathway is by decomposition of  $^{15}NO$  on Pt sites freed up by the storage of  $^{15}NO$  on the BaO phase by spillover.

Isotopic pump-probe experiments provide additional evidence of  $N_2$  formation on bulk Pt and also direct evidence of spillover processes during storage and reduction. Sequential pulses of  $^{15}NO$  and  $H_2$  were fed to a pre-nitrated Pt/BaO/Al<sub>2</sub>O<sub>3</sub> catalyst (using unlabeled NO); see Fig. 1. The data show the production of  $N_2$ ,  $^{15}N_2$ , and  $^{15}NN$  during  $^{15}NO$  and  $H_2$  pulses over 400 pump-probe cycles. Unlabeled  $N_2$  is produced by reverse NOx spillover from the Ba phase to Pt/BaO interface, where it decomposes to form  $N_2$ . The principal role of excess  $H_2$  is to scavenge oxygen adatoms formed during NO and  $^{15}NO$  decomposition, freeing up Pt sites. The excess hydrogen also reacts with NO or N at the Pt/Ba interfacial region to form NH<sub>3</sub>, causing a smaller production of  $N_2$  during the  $H_2$  pulse compared to  $^{15}NO$  pulse. As unlabeled  $NO_x$  is depleted from the Ba phase, the formation of  $N_2$  also declines. The formation of  $^{15}N_2$  is evident from the onset and is sustained throughout the experiment, indicating that decomposition

occurs on bulk Pt sites farther away from the Pt/BaO interface. In addition to N<sub>2</sub> and <sup>15</sup>N<sub>2</sub>, the mixed product <sup>15</sup>NN is formed during <sup>15</sup>NO pulse, providing evidence for the reverse spillover of stored NO<sub>X</sub> from the Ba phase to Pt sites where N and <sup>15</sup>N recombine. The production of <sup>15</sup>NN decreases at the expense of an increase in <sup>15</sup>N<sub>2</sub> as unlabeled stored NO<sub>X</sub> is depleted. Ongoing experimental results will be presented that elucidate the role of the Pt/BaO interface during NSR, such as NO<sub>X</sub> spillover from Pt to Ba phase and reverse spillover from Ba phase to Pt



**Figure 1.**  $N_2$ ,  $^{15}N_2$  and  $^{15}NN$  profiles during  $^{15}NO/H_2$  pump probe  $(H_2/^{15}NO = 4.4)$ on prenitrated (with NO) on Pt/BaO/Al<sub>2</sub>O<sub>3</sub> at 250 °C

## Significance

There is a need for reducing  $NO_X$  emissions from the exhaust of lean burn gasoline and diesel engines. This work is a step towards gaining a fundamental understanding of the complex catalytic chemistry of NSR through systematic transient experiments and the development of microkinetic models.