# Oxidative coupling of methane over Pb-substituted chlorapatite

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## Introduction

Although natural gas is an abundant resource, its utilization is limited due to the difficulties in storage/transportation and low chemical reactivity of its main component(CH<sub>4</sub>) for useful conversion. OCM(Oxidative coupling of methane) is usually regarded as one of the promising routes for utilizing natural gas(CH<sub>4</sub>) but the results are not satisfactory yet. Pb has been reported as a highly active catalytic component for OCM reaction[1]. High catalytic activity and thermal durability was reported when using Pb-substituted hydroxyapatites(Ca<sub>10</sub>, xPb<sub>x</sub>(PO<sub>4</sub>)<sub>6</sub>(OH)<sub>2</sub>,  $0 \le X \le 10$ , which will be abbreviated by Pb-HAp)[2]. The character of Pb-substituted Chlorapatite(Ca<sub>10-x</sub>Pb<sub>x</sub>(PO<sub>4</sub>)<sub>6</sub>Cl<sub>2</sub>,  $0 \le X \le 10$ , which will be abbreviated by Pb-ClAp) is similar to Pb-HAp. It is widely accepted that chlorine activate CH<sub>4</sub>. In this study, Pb-substituted chlorapatites were applied to OCM reaction, considering chlorine is effective for CH<sub>4</sub> activation.

## **Materials and Methods**

The Pb-ClAp catalysts were prepared by coprecipitation method. Starting solution was obtained by dissolving  $Ca(NO_3)_2$ ·4H<sub>2</sub>O, Pb(NO<sub>3</sub>)<sub>2</sub>, NH<sub>4</sub>Cl and (NH<sub>4</sub>)<sub>2</sub>HPO<sub>4</sub> in distilled water. During the mixing, the pH of the mixure was adjusted 9 by addition of aqueous ammonia. After mixing, mixture was stirred at 90°C for aging. Then the matured suspension was dried and calcined[2]. The measurements for activity of the catalysts performed with atmospheric pressure fixed bed reactor. Reactivity of the catalysts investigated with on-line GC.

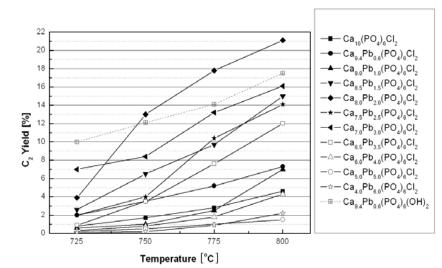
### **Results and Discussion**

Since OCM reaction is carried out usually at high temperature, the maintenance of Pb, which is highly volatile, is important as well as the activity of the catalyst. Therefore, it was necessary to investigate whether ClAp hold Pb effectively. PbO/Al<sub>2</sub>O<sub>3</sub>, used as catalyst for OCM by Roos et al.[3], was adopted for comparison. Table 1 showed that the change of atomic concentration in Pb-ClAp and PbO/Al<sub>2</sub>O<sub>3</sub> by ICP-AES analysis. Unlike Pb in PbO/Al<sub>2</sub>O<sub>3</sub>, Pb in ClAp was maintained its initial concentration for 40 hours.

#### Table 1. ICP-AES analysis of Pb-ClAp and PbO/Al<sub>2</sub>O<sub>3</sub>

	Catalyst	Ratio	Intended	Fresh	10 hr	20 hr	30 hr	40 hr
	Ca <sub>7.5</sub> Pb <sub>2.5</sub> (PO <sub>4</sub> ) <sub>6</sub> Cl <sub>2</sub>	Ca/Pb	3.0	2.7	2.7	2.8	2.6	2.7
		Pb/P	0.4	0.5	0.5	0.4	0.5	0.4
	PbO/Al <sub>2</sub> O <sub>3</sub>	Al <sub>2</sub> /Pb	1.0	N.A	1.0	1.2	3.3	N.A

The C<sub>2</sub> yield of Pb-ClAps is shown in Fig. 1. At 800  $^{\circ}$ C, Ca<sub>8.0</sub>Pb<sub>2.0</sub>(PO<sub>4</sub>)<sub>6</sub>Cl<sub>2</sub> showed 21.1% C<sub>2</sub> yield. As compared to Ca<sub>9.4</sub>Pb<sub>0.6</sub>(PO<sub>4</sub>)<sub>6</sub>(OH)<sub>2</sub> that prepared by coprecipitation[2], Ca<sub>8.0</sub>Pb<sub>2.0</sub>(PO<sub>4</sub>)<sub>6</sub>Cl<sub>2</sub> showed much higher C<sub>2</sub> yield.



**Figure 1.** Catalytic activities of Pb-ClAp catalysts (catalyst 0.36g, total flow rate 37ml/min, CH<sub>4</sub>:O<sub>2</sub>:He=8:4:25, W/F= $1.6 \times 10^{-4}$ g<sub>cat</sub>·hr/ml)

# Significance

As compared to Pb-HAp, Pb-ClAp showed much C<sub>2</sub> selectivity in OCM reaction.

	Temp.(℃)	Catalyst	CH <sub>4</sub> Conv.(%)	C <sub>2</sub> Sel.(%)	C <sub>2</sub> Yield(%)			
	750	Ca8.5Pb1.5-HAp	15.3	26.2	4.0			
		Ca8.5Pb1.5-ClAp	15.2	42.7	6.5			
	775	Ca8.5Pb1.5-HAp	19.8	24.7	4.9			
		Ca8.5Pb1.5-ClAp	20.8	46.4	9.7			
	800	Ca8.5Pb1.5-HAp	23.7	26.5	6.3			
		Ca8.5Pb1.5-ClAp	30.5	49.1	15.0			

Table 2. The comparison of Pb-HAp and Pb-ClAp in catalytic activity

### References

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