

Using Calcium Oxide Based Catalysts in Transesterification of Soybean Oil with Methanol

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Introduction

Biodiesel, a renewable fuel with similar combustion properties to fossil diesel, is normally produced by the transesterification of highly refined oils with short-chain alcohols. Conventionally, some homogeneous base catalysts such as NaOH and NaOCH₃ were employed. However, these homogeneous catalysts are corrosive. And removal of these catalysts after reaction causes a large amount of waste wash water and a long time for phase separation. Moreover, traditional base catalysts can react with water and free fatty acids (FFA) in feedstocks to form soap which will greatly decrease the catalyst activity. Therefore, highly refined acid-free oil (FFA content < 0.5 %, water content < 0.06%) and anhydrous alcohol should be used for homogeneous base catalysts. However, that leads to a high feedstock cost. Thus, new catalytic processes are desirable for the development of an environmentally benign process, which can utilize low cost unrefined and waste oils directly.

Heterogeneous basic catalysts such as supported alkaline metal hydroxide catalysts [1] and alkaline earth metal oxide catalysts[2] have been studied. However, most of the reported heterogeneous catalysts show a much lower activity than traditional homogeneous base catalysts. Recently Yan et al. [3] reported a supported CaO catalyst have a high activity and an improved tolerance to water (2 %) and FFA (3 %). However, effects of water and FFA on catalyst structure and the catalytic performance in unrefined and waste oils were not fully elucidated. In this study, a lanthanum modified CaO catalyst was prepared and used in unrefined and waste oil system for biodiesel production. The effects of catalyst structure and reaction parameters (water and FFA content, oil feedstock types, water and CO₂ in air, molar ratio of methanol to oil, reaction temperature, activation temperature and catalyst dosage) on the yield of fatty acid methyl esters (FAME) were studied.

Materials and Methods

A sol-gel method was used to prepare calcium oxide based catalysts (Ca₃La₁, Ca₁La₀ and Ca₀La₁). Catalysts were characterized by XRD, XPS, SEM and EDS measurements. Reaction was performed in a batch reactor. In most studies, 10.0 g of soybean oil and 7.6 g of methanol and 0.5 g activated oxide catalyst were used.

Results and Discussion

Table 1 shows that Ca₃La₁ is a mixture of CaO, La₂O₃ and La(OH)₃ phases. And the average crystal size of CaO is about 57.2 nm. Ca₃La₁ has a stronger base strength and a higher amount of basicity than Ca₁La₀ and Ca₀La₁. Moreover, Ca₃La₁ has the highest specific BET surface area and FAME yield.

Crude soybean oil, crude palm oil and waste cooking oil without any pretreatment were converted to FAME directly using Ca₃La₁ catalyst (Figure 1). The average yield of these oils was about 96 % at 3 hours.

Table 1. Specific surface areas, XRD, basicity and catalytic activity of Ca₁La₀, Ca₀La₁, Ca₃La₁

| Catalyst | BET Area m ² /g | X-ray Structure | Basicity mmol/g | | | | Total Basicity mmol/g | Yield of FAME % ¹ |
|---------------------------------|----------------------------|---|-----------------|------------|------------|-----------|-----------------------|------------------------------|
| | | | 4.2<H.<6.8 | 6.8<H.<7.2 | 7.2<H.<9.8 | 9.8<H.<15 | | |
| Ca ₁ La ₀ | 10.4 | Ca(OH) ₂ | 0.3 | 0.1 | \ | \ | 0.4 | 18.7 |
| Ca ₀ La ₁ | 9.9 | La(OH) ₃ | 0.1 | \ | \ | \ | 0.1 | 3.2 |
| Ca ₃ La ₁ | 62.6 | CaO, La ₂ O ₃ , La(OH) ₃ | 0.6 | 2.0 | 10.4 | 1.0 | 14.0 | 95.3 |

Significance

This class of catalysts can directly utilize waste or unrefined oils and it provides a potential to decrease the production cost and feedstock cost of biodiesel.

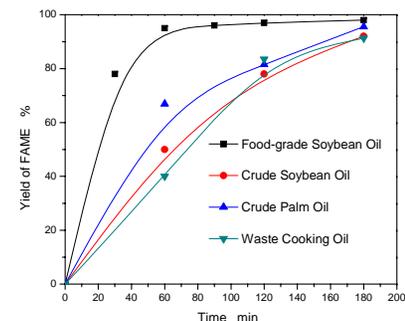


Figure 1. FAME yield of crude palm oil, crude soybean oil, waste cooking oil, food-grade soybean oil

References

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